Large-Scale Synthesis of TiO₂ Microspheres with Hierarchical Nanostructure for Highly Efficient Photodriven Reduction of $CO₂$ to $CH₄$

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S Supporting Information

[AB](#page-8-0)STRACT: [In this study,](#page-8-0) a simple and reproducible synthesis strategy was employed to fabricate $TiO₂$ microspheres with hierarchical nanostructure. The microspheres are macroscopic in the bulk particle size (several hundreds to more than 1000 μ m), but they are actually composed of P25 nanoparticles as the building units. Although it is simple in the assembly of P25 nanoparticles, the structure of the as-prepared $TiO₂$ microspheres becomes unique because a hierarchical porosity composed of macropores, larger mesopores (ca. 12.4 nm), and smaller mesopores (ca. 2.3 nm) has been developed. The interconnected macropores and larger mesopores can be utilized as fast paths for mass transport. In addition, this hierarchical nanostructure may also contribute to some extent to the enhanced photocatalytic activity due to increased multilight reflection/scattering. Compared with the state-of-the-art photocatalyst, commercial Degussa P25 TiO₂, the as-prepared TiO₂ microsphere catalyst

has demonstrated significant enhancement in photodriven conversion of $CO₂$ into the end product CH₄. Further enhancement in photodriven conversion of CO_2 into CH_4 can be easily achieved by the incorporation of metals such as Pt. The preliminary experiments with Pt loading reveal that there is still much potential for considerable improvement in $TiO₂$ microsphere based photocatalysts. Most interestingly and significantly, the synthesis strategy is simple and large quantity of TiO₂ microspheres (i.e., several hundred grams) can be easily prepared at one time in the lab, which makes large-scale industrial synthesis of $TiO₂$ microspheres feasible and less expensive.

KEYWORDS: TiO₂ spheres, hierarchical nanostructure, Pt loading, photocatalyst, CO₂ reduction

1. INTRODUCTION

Although carbon dioxide is the least potent of all the greenhouse gas (GHG) emissions, it is the most important in terms of its contribution to climate change. The rapid increase in the level of anthropogenic $CO₂$ resulting in global climate change is a matter of great concern. Turning $CO₂$ into a clean energy fuel would be a solution for both the shortage of fossil fuels and the global warming problem. Hence, this is an energy research topic of great interest. However, the process for turning $CO₂$ into fuels is energy intensive and useful only if a renewable energy source can be used for the purpose. Therefore, a potential avenue for sustainable development is to use photocatalysts for the conversion of $CO₂$ into hydrocarbon fuels with the help of solar energy, a clean and renewable energy source.

Titania has been considered a particularly appropriate candidate for photocatalytic processes due to its powerful oxidation properties, superior charge transport properties, and corrosion resistance.^{1−12} Furthermore, it is readily available and less expensive compared with other photocatalyst candidates such as gallium-phosphide semiconductors^{13,14} and transition metal complexes, such as ruthenium(II) polypyridine carbonyl $complex,$ ¹⁵ cobalt(II) trisbipyridine,¹⁶ and [rhen](#page-8-0)ium(I) bipyridine (bpy) complexes, fac- $[Re(bpy)(CO)_3L]$ (L = SCN- (1-NCS), [Cl-](#page-8-0) (1-Cl), and CN- $(1-CN)$.¹⁷ Due to its attractive properties such as nontoxicity, high availability, low cost, and long-term stability against photo and c[hem](#page-8-0)ical corrosion, titania has attracted much attention in recent years as a photocatalyst in "artificial photosynthesis", i.e., photoassisted water splitting^{18,19} and CO_2 conversion.²⁰ Other applications include the degradation of organic pollutants,⁸ water disinfection and puri[fi](#page-8-0)[cat](#page-8-0)ion, hazardous wast[e](#page-8-0) remediation, and air purification.^{21,22} Various TiO₂-based mater[ia](#page-8-0)ls have been investigated for photoassisted $CO₂$ conversion, but to date, mainly com[mer](#page-8-0)cial Degussa P25²³⁻²⁵ and TiO₂ nanotubes $(NTs)^{26,27}$ have been used. However, these TiO₂-based

Receiv[ed:](#page-9-0) June 26, 2014 Accepted: August 20, 2014 Published: August 20, 2014 materials are either time-consuming and costly to produce $26,27$ and/or cannot efficiently drive the $CO₂$ conversion reaction without an appropriate co-catalyst due to the wide energy [gap](#page-9-0) of TiO_2 .^{23–25} Incorporating transition metals is an effective method to tailor and engineer the structure, phase, and band gap. Co[pper i](#page-9-0)s considered as one of the most suitable options since both cupric oxide and cuprous oxide are p-type semiconductors with a narrower band gap.²⁸ Additional promising metals for dopants are Fe^{29} and Sn^{30} .

In addition to the problem caused by the wid[e e](#page-9-0)nergy gap of $TiO₂$, low photocatalytic activity for $TiO₂$ -bas[ed](#page-9-0) materials can result from the recombination of the electron−hole pairs generated by photo irradiation. Generally, the electron−hole pairs generated by solar irradiation and their lifetime are key factors for the photocatalytic reaction and efficiency. Titania has so far yielded only low carbon dioxide conversion rates despite using ultraviolet illumination for band gap excitation,²⁶ which is not practical for the commercialization of $CO₂$ reduction. Therefore, considerable enhancement in photocatal[ytic](#page-9-0) activity of TiO₂-based photocatalyts is required. An efficient approach to reduce the recombination rate of the electron−hole pairs is to disperse $TiO₂$ onto a substrate (i.e., support) such as carbon NTs, which function as dispersing agents to prevent the $TiO₂$ nanoparticles (NPs) from agglomerating and hence decrease the recombination rate of the electron−hole pairs.³¹ Other strategies include doping noble metals such as $Ru₃³² Pd₂^{33,34}$ or Pt^{26} onto $TiO₂$, which can change the distribution of [ele](#page-9-0)ctrons and effectively prevent the electron−hole recomb[ina](#page-9-0)tio[n.](#page-9-0)

[C](#page-9-0)urrent photocatalysts for $CO₂$ reduction are inefficient. State-of-the-art $CO₂$ photoreduction catalysts do not perform as efficiently as the state-of-the-art catalysts for H_2 photogeneration.³⁵ Therefore, it is highly desirable to develop novel photocatalysts with high catalytic activity toward $CO₂$ photoreduction. [R](#page-9-0)ecently, Wang et al. reported photoreduction of $CO₂$ using $CdSe/Pt/TiO₂$ heterostructured catalysts.³⁶ Although costly catalysts were utilized and complicated synthesis procedures involved, due to the irradiation un[der](#page-9-0) visible light, photoreduction efficiency of $CO₂$ was still low compared with that obtained under UV irradiation. More recently, Liu et al. reviewed engineering $TiO₂$ nanomaterials for $CO₂$ conversion,³⁷ and Mori et al. commented on photocatalytic reduction of CO_2 with H_2O on various titanium oxide photocatalysts.³⁸

In this study, novel $TiO₂$ -based spherical photocatalysts with large mesop[oro](#page-9-0)us volume and hierarchical porosity are designed and developed to improve the photocatalytic activity and efficiency for solar reduction of $CO₂$. The synthesis strategies for the $TiO₂$ spheres and Pt-loaded ones are relatively simple, scalable and reproducible. Interestingly, compared with the widely used benchmark photocatalyst, commercial Degussa P25 TiO₂, the TiO₂ microsphere photocatalyst demonstrates remarkably enhanced photocatalytic activity toward photodriven $CO₂$ reduction to $CH₄$ due to its large surface area and particularly the unique hierarchical porosity, facilitating fast mass transport. In addition, the hierarchical nanostructure may also contribute to the improved photocatalytic activity due to enhanced multilight reflection/scattering. Furthermore, further improvement in photodriven conversion of $CO₂$ can be realized readily through a simple approach, incorporation of metals such as Pt.

Compared with nanosized $TiO₂$ catalysts reported by other researchers, the $TiO₂$ microspheres with larger particle size (several hundreds to more than 1000 μ m) developed in this

study are self-supported (i.e., they do not need a supporting substrate). The $TiO₂$ microspheres possess advantages over other nanoscaled materials, such as commercial P25 NPs. The $TiO₂$ microspheres with macroscopic particle size do not have a particle agglomeration issue, making handling much simpler (i.e., no need to make pellets or to make a thin film on a substrate). From the viewpoint of some practical applications, the $TiO₂$ microspheres catalyst is a very good functional material design, making large-scale synthesis and application of photocatalyst feasible. Furthermore, this photocatalyst possesses excellent mechanical strength, 39 and thus is better suited for a fluidization bed reactor which is an inherently scalable and favorable reactor for industrial use.

2. EXPERIMENTAL SECTION

2.1. Synthesis of Photocatalysts. $TiO₂$ spheres with large particle size (greater than 500 μ m) were synthesized through a modified TiO_2° sol−gel approach^{18,39} as illustrated in Figure 1.

Figure 1. Illustration for the synthesis of $TiO₂$ spheres.

Typically, 96 mL of C_2H_5OH was mixed with 6.4 mL of deionized H2O (DI), followed by the addition of 16 mL of concentrated HCl (Fisher, 37%) and 120 mL of titanium isopropoxide (TTIP) (Sigma-Aldrich, 97%) while the solution was vigorously stirred. After the solution stirred for 2 h at 360 rpm, 38 g of precalcined Degussa P25 powder was then introduced to the sol−gel solution and the resulting P25 in Ti(IV) sol−gel was stirred overnight. Next, a chitosan glacial acetic acid aqueous solution (1 wt %) was introduced to the sol−gel in the volume ratio of 2:1. After it stirred for 2 h, the resulting mixture was then added dropwise from a modified buret into a basic $NH₄OH$ (Fisher, 30%) aqueous solution (6 vol %). TiO₂ spheres were produced and collected from the basic solution and calcined at 450 °C for 3 h. In the synthesis, commercial P25 $TiO₂$ was dispersed in the sol as filler to fabricate composite high performance sol−gel materials. P25 $TiO₂$ was chosen because of its high photoefficiency to degrade organic pollutants.

Pt-loaded TiO₂ spheres with various Pt contents were prepared through a microwave-assisted synthesis strategy using ethylene glycol (EG) as the reducing agent.40−⁴² The Pt-loaded catalysts were thoroughly washed with ethanol and DI water to remove any residual EG.

2.2. Physical Characteriz[ation](#page-9-0). N_2 adsorption and desorption isotherms were measured at 77 K on a Micromeritics ASAP-2020 Gas Adsorption Analyzer after a sample was degassed at 423 K to 20 mTorr for 12 h. The specific surface areas were determined from nitrogen adsorption using the Brunauer−Emmett−Teller (BET) method. Total pore volumes (V_{Total}) were determined from the amount of gas adsorbed at a relative pressure of 0.99. Micropore volume (V_{Micro}) and micropore size of the porous materials were calculated from the analysis of the adsorption isotherms using the Horvath−Kawazoe (HK) method. Pore size distribution (PSD) was calculated from the adsorption branches by the Barrett−Joyner− Halenda (BJH) method.

A

 $\, {\bf B}$

Surface morphologies of the various $TiO₂$ -based catalysts were examined by a scanning electron microscope (SEM) FEI Helios NanoLab 650 FIB-SEM or by a Cameca SX-50 Scanning Electron Microprobe with 4 vertical wavelength-dispersion X-ray spectrometers and a fully integrated SAMx energy-dispersion X-ray spectrometer.

X-ray diffraction (XRD) patterns were obtained on a Siemens D5000 (Vantec detector) and Bruker D8 Focus (LynxEye detector) Xray powder diffractometers by using Co K α radiation as the X-ray source, operating at 35 kV and 40 mA. The diffractograms were recorded in the 2θ range 10−80°, in steps of 0.02° with a count time of 20 s at each point. The particle size was determined from the broadening of the diffraction peak using the Scherrer formula, $D = K\lambda$ / β cos θ , where D is the crystallite size (nm), K is the Scherrer constant, λ is the wavelength of the X-ray source, $β$ is the full width at halfmaximum, and θ is the Bragg angle.

X-ray photoelectron spectroscopy (XPS) measurements were made with a Leybold MAX200 spectrometer using a Mg K α source (1253.6) eV) operated at 15 kV and 20 mA. All binding energies were corrected for sample charging by referencing to the adventitious C 1s peak at 285.0 eV.

A Varian Cary 4000 UV−visible diffuse reflectance spectrophotometer was employed to obtain UV−visible diffuse reflectance spectra (UV−vis DRS) for various photocatalysts over a spectral range of 200−800 nm.

2.3. Photodriven Reduction of $CO₂$ **.** The use of titania and water (without sacrificial hole scavengers) ultimately provides a green chemistry approach for the photoconversion of \hat{CO}_2 to fuels.^{43,44} In this study, water was used as the only electron donor.

A batch reactor of 39 mm in diameter and 9 mm in depth w[as ma](#page-9-0)de for photocatalytic conversion of $CO₂$ with water. For a typical run, a mixture of 200 mg of catalyst mixed with 100 μ L of H₂O was placed in a container (20 mm in diameter) located in the center of the reactor. After the introduction of pressurized CO_2 (50 PSI) (or N_2 , for blank experiments only; will be explained later in this section), the reactor was irradiated with a Hg UV lamp (40 W, 254 nm, light intensity at the location of catalyst: 20 mW cm[−]²) for a 24 h period. The gas products were collected through a 10 mL syringe and injected into a gas chromatograph (SRI 8610 Gas Chromatograph, Mandel, Canada), which was equipped with FID and TCD detectors for the detection of CH_4 , CO, and H₂, respectively. Because this study focused on CO_2 photoreduction on a gas−solid interface, possible liquid products like methanol, formaldyhyde and formic acid, which are more likely generated in aqueous solutions, were not measured. For each type of catalyst, experiments were carried out at least three times using fresh catalyst each time. The production rates are averaged and reported with standard deviations.

Stability tests were conducted for the used photocatalysts after being removed from the reactor followed by storage in air at room condition for 24 h. Then, the used photocatalysts were placed back in the reactor without further treatment.

Prior to any photocatalytic conversion of $CO₂$ with water, all the reported catalysts in this study had been examined in blank experiments to make sure that there was no carbon-containing product produced without introduction of $CO₂$ into the reactor. The results from the blank experiments confirm that the carbon-containing gas products (i.e., CO, CH_4 , etc.) were produced from the photoreduction of $CO₂$ only, not from residual carbon-containing organics in the catalysts.

The digital photographs for the experimental setup are shown in Figure S1 (Supporting Information).

3. RESU[LTS AND DISCUSSI](#page-8-0)ON

Figure 2 shows digital photograph and representative SEM images for the as-prepared $TiO₂$ spheres. As shown in Figure 2A, the $TiO₂$ spheres take on a yellowish color. The SEM image in Figure 2B reveals that the $TiO₂$ spheres have a diameter of ca. 1.3 mm, and generally, the outer surface of the sphere is

 $500 \ \mu m$ Acc.V Spot Magn Det WD 15.0 kV 6.0 174x **BSE 10.9**

Figure 2. Digital photograph (A), and SEM images with various magnifications (B and C) for the as-prepared $TiO₂$ spheres.

smooth. The magnified image (Figure 2C) shows that the most of the outer surface is densely packed with small particles of ca. 12−28 nm. In some areas, larger particles of ca. 58−86 nm were also observed. In addition, mesopores (voids) in the range from ca. 10 to 50 nm are clearly observed, which are formed by the aggregated particles. Interestingly, it was also found that through controlling the rate for the addition of the mixture of P25 in Ti(IV) sol−gel into the ammonia solution, the particle size of the obtained $TiO₂$ spheres could be effectively

controlled, as shown in Figure S2 (Supporting Information). In contrast, the commercial Degussa P25 shows the agglomeration of TiO2 NPs of ca. 15−50 nm[, as evident in Figure](#page-8-0) S3 (Supporting Information).

Representative nitrogen adsorption−desorption isotherms for the as-prepared $TiO₂$ spheres (ca. 1.3 mm in diameter) are shown in Figure 3A. They can be classified as a type IV

Figure 3. Representative nitrogen adsorption−desorption isotherms at 77 K and derived PSD for the as-prepared $TiO₂$ spheres (A) and commercial P25 TiO₂ (B).

isotherm with a type H2 hysteresis loop, according to the BDDT (Brunauer, Deming, Deming and Teller) classification. The $TiO₂$ spheres sample reveals a BET surface area of ca. 50.2 m^2 g⁻¹, a mesoporous volume of ca. 0.253 cm³ g⁻¹ and a negligible micorporous volume. Interestingly, the sample demonstrates a hierarchical porosity composed of macropores (greater than 50 nm), larger mesopores with a PSD maximum located at ca. 12.4 nm, and smaller mesopores of ca. 2.3 nm. The pore size measured by the BET measurement is in good agreement with that observed from the SEM image shown in Figure 2C. As shown in Figure 3B, the P25 $TiO₂$ sample shows a type H3 hysteresis, indicating the presence of mesopores. The PSD r[ev](#page-2-0)eals that P25 has a single size distribution with a PSD maximum located at ca. 2.6 nm, which is much smaller that the larger mesopores (ca. 12.4 nm) observed for the $TiO₂$ spheres. The P25 TiO₂ has a BET surface area of ca. 48.4 $\text{m}^2 \text{ g}^{-1}$, which

is slightly smaller than that of the as-prepared $TiO₂$ spheres. In addition, the P25 sample has a mesoporous volume of ca. 0.180 $\text{cm}^3 \text{ g}^{-1}$, which is significantly smaller than that (i.e., 0.253 cm^3 g^{-1}) measured for the TiO₂ spheres, and also a negligible microporous volume. The larger surface area and mesoporous volume, and particularly the hierarchical porosity, would be expected to improve the photocatalytic activity of the $TiO₂$ spheres catalyst.

To further enhance photocatalytic conversion efficiency, the as-prepared $TiO₂$ spheres were decorated with Pt. SEM images for some representative Pt-incorporated $TiO₂$ sphere catalysts are shown in Figure 4. It is evident that with increasing Pt content there is more coverage of the outer surface of the $TiO₂$ spheres with Pt particl[es](#page-4-0), which grow in size and result in some agglomeration. When the Pt content is as low as 0.3 wt %, the Pt NPs size is ca. 5−10 nm (Figure 4A), while the size increases to 8−16 nm (Figure 4B) when the Pt content reaches 0.6 wt %. Although the size increases, Pt NP[s](#page-4-0) still disperse uniformly on the substrate. Ho[we](#page-4-0)ver, when the Pt content is further increased to 0.9 wt %, the size of the Pt NPs increases significantly and reaches 18−22 nm (Figure 4C) with some agglomeration. When the Pt content increases to 1.8 wt %, Pt NPs are found to have a mean size of ca. 24 [nm](#page-4-0) as shown in Figure 4D and Figure S4 (Supporting Information), which is ca. twice that observed for the Pt $(0.6 \text{ wt } \%) / TiO₂$. Interestingly, compa[re](#page-4-0)d with Pt $(1.8 \text{ wt } \%) / TiO_2$, the Pt NPs in Pt $(0.6 \text{ wt } \%)$ %)/TiO₂ have a much smaller particle size (average ca. 12 nm) and a more uniform dispersion on the $TiO₂$ surface, as shown in Figure 4B.

XRD data shown in Figure 5A reveals the $TiO₂$ spheres catalyst h[as](#page-4-0) a similar pattern to that of the commercial P25 sample except that the former re[ve](#page-5-0)als stronger diffraction peaks for the anatase phase, suggesting larger crystalline size. The data also reveal that the $TiO₂$ spheres catalyst consists of 79% anatase $TiO₂$ with a crystalline size of 19 nm and 21% rutile $TiO₂$ with a crystalline size of 75 nm. Thus, the dominant phase in the $TiO₂$ spheres is anatase, similar to P25. XRD patterns for the Pt-incorporated $TiO₂$ spheres with various Pt contents are shown in Figure 5B. For a clear comparison and better understanding, Pt black was also characterized by XRD measurement, and [th](#page-5-0)e data is shown in Figure S5 (Supporting Information). It was found that in the scanned range, Pt has a reflection peak Pt(111) located at 46.6° and a refl[ection peak](#page-8-0) [Pt\(200\) loca](#page-8-0)ted at 54.4 °. However, from Figure 5, only anatase and rutile $TiO₂$ phases were observed for the Pt-loaded $TiO₂$ samples, and no separate Pt-related reflection p[ea](#page-5-0)k was shown even for the Pt $(1.8 \text{ wt } \%) / TiO₂$. This phenomenon has been reported for Pt-incorporated TiO_2 materials when Pt contents are lower than 4 wt %. $45,46$ This can be explained because $Pt(IV)$ has an ionic radii of 0.625 Å, which is comparable to that of $Ti(IV)$ (0.605 Å)[. Thu](#page-9-0)s, it is energetically favorable for Pt ions to occupy $Ti(IV)$ sites.⁴⁷ In addition, the Pt loadings may be too low to be detected by laboratory-based XRD with a typical detection limit of 5 wt [%.](#page-9-0)

XPS data shown in Figure 6A reveal that P25 $TiO₂$ and the $TiO₂$ spheres are composed of pure $TiO₂$. For the Pt-loaded sample, the peaks for Pt 4d a[nd](#page-5-0) 4f are clearly observed even for the sample with low Pt content (i.e., 0.3 wt %). The doublet peaks shown in the magnified Pt 4f spectrum (Figure 6B) were observed at 71.2 and 74.6 eV, which are attributable to 4f7/2 and 4f5/2 of metallic Pt, respectively, implying [t](#page-5-0)hat the dominant valences of the Pt species in the catalysts are zero. After the deconvolution of the magnified XPS spectrum for Pt

Figure 4. SEM images for the Pt-TiO₂ spheres catalysts with various metal loadings: (A) 0.3, (B) 0.6, (C) 0.9, and (D) 1.8 wt %.

4f, it was also found that the deposited Pt NPs on the outer surface of the Pt $(0.3 \text{ wt } \%) / TiO₂$ are composed of 76% of Pt (0), 16% of Pt (II) and 8% of Pt (IV).

Various $TiO₂$ -based catalysts were investigated for photodriven $CO₂$ reduction with water. Table 1 summarizes yields of the gas products for the P25 and spherical $TiO₂$ photocatalysts without Pt loading.

The P25 catalyst shows a production [yi](#page-5-0)eld of 0.20, 2.31, and 1.72 µmol g(catalyst)⁻¹ h⁻¹ for CH₄, CO, and H₂, respectively, while the as-prepared $TiO₂$ spheres catalyst produces 0.94, 2.32, and 2.03 μ mol g⁻¹ h⁻¹ of CH₄, CO, and H₂, respectively. Intermediate product CO is identified as the major carboncontaining gas product for the photodriven reduction of $CO₂$ with H_2O for the plain TiO_2 catalysts, which has also been observed by other researchers.^{48,49} In addition, it was also found that when P25 and the plain $TiO₂$ spheres were used as a photocatalyst, no C_2H_6 , ethyle[ne, o](#page-9-0)r acetylene was detected. The phenomenon observed for the commercial P25 is consistent with that reported by Tan et $al.^{24}$ It is well-known that $CH₄$ is the end product for the photocatalytic reduction of $CO₂$, [an](#page-9-0)d thus, it has more significance than the intermediate products like CO. The as-prepared $TiO₂$ microsphere catalyst and commercial P25 catalysts are very close in specific surface area, as revealed by the BET measurements. Therefore, the enhanced selectivity of $CH₄$ production observed for the asprepared $TiO₂$ microsphere catalyst is mainly attributable to the larger mesoporous volume and particularly the hierarchical pore structure composed of macropores, larger mesopores (ca. 12.4 nm) and smaller mesopores (ca. 2.3 nm). Compared with the commercial P25 NPs catalyst, the as-prepared $TiO₂$ microsphere catalyst is advantageous and superior because numerous meospores with large pore size have been developed

throughout the whole microsphere during the assembly of P25 NPs. These large mesopores can be considered as hollow channels, facilitating fast mass transport within the $TiO₂$ microsphere. Zhao et al. reported that the multichannel hollow structure in $TiO₂$ fibers induces not only an inner trap effect on gaseous molecules, but also a multiple-reflection effect on incident light, which further improves the photocatalytic activity of TiO2 hollow fibers.⁵⁰ Therefore, the hierarchical nanostructure developed in the $TiO₂$ microsphere not only favors fast mass transport, result[ing](#page-9-0) in enhanced photocatalytic activity, but may also contribute to the improved photocatalytic activity due to the enhanced multilight scattering. This creates a greater possibility for multielectron reaction, i.e., eight electrons for CH_4 generation. Thus, the as-prepared TiO_2 microsphere is completely different from other $TiO₂$ bulk materials without highly developed mesopores, in which only a few micrometers of the $TiO₂$ outer surface can be utilized for light harvesting, resulting in low photodriven $CO₂$ conversion into $CH₄$. Clearly, the $TiO₂$ microspheres have particularly unique features: they not only maintain the nanoscale properties from the building units of P25 TiO₂ NPs, but also benefit from additional collective properties at the macroscopic scale, namely, the hierarchical porosity developed during the assembly of $TiO₂$ NPs. Other researchers have also suggested that hierarchical nanostructures for photocatalysts improve photocatalytic activity. Zhu et al. reported that the hierarchical structures of photocatalysts contribute significantly to the absorption enhancement under visible light.^{51,52} Wang et al. also reported that nanoporous $SnO₂$ catalyst containing two types of porous structures has higher photocatal[ytic](#page-9-0) activity than Degussa P25 for degrading methyl orange.⁹ Li et al. reported that the

Figure 5. XRD patterns for plain $TiO₂$ samples (A), and for Pt incorporated $TiO₂$ spheres with various metal contents (B).

multilight scattering demonstrated by hierarchical nanostructured $TiO₂$ contributes to enhanced photocatalytic activity.^{53,54}

After the exposure to ambient air in the room environment for 24 h, the used photocatalysts show slightly decre[ased](#page-9-0) production yields for all the gas products, resulting from the accumulation of carbonaceous compounds. A similar phenomenon has also been observed by other researchers for $TiO₂$ based photocatalysts employed for photodriven $CO₂$ reduction with H_2O^{48} However, the results from the stability tests indicate that the used catalysts have been largely regenerated during am[bie](#page-9-0)nt air exposure due to desorption of the gas products from the surface of the catalysts.

Pt has been frequently used as a photocatalytic promoter, which can effectively change the distribution of electrons and reduce the electron−hole recombination reaction.²⁶ Figure 7 shows the data obtained for the spherical $TiO₂$ catalysts with various Pt loadings.

Compared with the P25 catalyst, the plain $TiO₂$ spher[es](#page-6-0) catalyst shows greatly enhanced photocatalytic activity toward the reduction of $CO₂$, i.e., about 5 times as much $CH₄$ is produced by the plain $TiO₂$ spheres catalyst. After Pt loading, the $TiO₂$ spheres catalyst produces an even higher concentration of H_2 because Pt prevents the recombination of electron−hole pairs, which in turn increases the photocatalytic

Figure 6. XPS spectra for the various $TiO₂$ based catalysts (A), and the deconvolution of Pt 4f doublet for Pt $(0.3 \text{ wt } \%) / TiO_2$ spheres (B) .

Table 1. Yield $(\mu \text{mol g}(\text{catalyst})^{-1} \ \text{h}^{-1})$ of the Gas Products $(H₂, CO, and CH₄)$ Produced during 24 h of Photodriven $CO₂$ Reduction on the Various Pure TiO₂ Catalysts^a

gas	P ₂₅		$TiO2$ spheres	
product	fresh	used ^b	fresh	used ^b
CH ₄	0.20	0.18	0.94	0.87
CO	2.31	1.98	2.32	2.06
Н,	1.72	1.56	2.03	1.95

 a Experimental conditions: 200 mg of catalyst mixed with 100 μ L of DI $\frac{L}{L}$ and $\frac{L}{L}$ is the state of $\frac{L}{L}$ of $\frac{L}{L}$ and $\frac{L}{L}$ and catalyst means it has been run for one test.

production of H_2 . It was reported that H_2 can work as another reductant to facilitate the reduction of $CO₂$ to $CH₄$. Lo et al. reported that hydrogen molecules can be adsorbed dissociatively to form H^+ on the surface of $TiO₂$ and supplied as a hydrogen atom to convert $CO₂$ to hydrocarbons by photoreduction.²³ H⁺ would further react with an e⁻ to produce \cdot H

Figure 7. Yields of the gas products $(H_2, CO \text{ and } CH_4)$ produced during 24 h of photodriven CO_2 reduction on TiO_2 sphere catalysts with various Pt loadings. Experimental conditions: 200 mg of catalyst mixed with 100 μ L of DI water, pressurized CO₂ (50 PSI), UV (20 mW/cm² , 254 nm).

radicals. The • H radicals are a highly reactive species, which directly react with $CO₂$ and accelerate its reduction. Therefore, it is clear that with the increasing H_2 content, the CH₄ produced is expected to increase. Due to the much larger amount of H_2 produced by the Pt-loaded TiO₂ catalysts, more $CH₄$ is produced. As seen from Figure 7, the amount of $CH₄$ and CO produced by the Pt-loaded $TiO₂$ catalysts is higher than that produced by the plain $TiO₂$ catalysts (i.e., P25 and $TiO₂$ spheres), which indicates that Pt-loaded $TiO₂$ catalysts have much higher catalytic activity toward the solar reduction of $CO₂$ than the plain ones.

In addition, other hydrocarbons such as C_2H_6 and/or C_2H_4 have also been reported to be produced through other reaction paths²³ when the H₂ concentration is high in the reaction system. This explains why C_2H_6 and C_2H_4 were produced by the [Pt-l](#page-9-0)oaded $TiO₂$ catalysts. It is also interesting to note that the H_2 and CH₄ amounts produced by the Pt-loaded TiO₂ catalysts increase with increasing Pt content up to 0.6 wt %, and

then decreased with a further increase in the Pt content. While the addition of platinum allows the hydrogen evolving reaction to proceed, platinum deposits also catalyze the back reaction of hydrogen and oxygen to form water and heat, which becomes dominant at some level of Pt loading, thus reducing the overall efficiency of the system.^{18,51} In addition, with an increase in the Pt loading, Pt NPs increase in size, resulting in worse particle di[sp](#page-9-0)ersion on the $TiO₂$ spheres substrate, which not only lowers the catalytic efficiency of Pt, but also results in lower light harvesting due to the shadowing of the photocatalyst particle $(TiO₂)$ by surface platinum deposits. This is evident from the comparison of the SEM images shown in Figure 4B for Pt $(0.6 \text{ wt } \%) / TiO₂$ and Figure S4 for Pt $(1.8 \text{ wt } \%) / TiO₂$. From Figure S4 it was found that most of the surface of [th](#page-4-0)e $TiO₂$ particles is covered by [the Pt N](#page-8-0)Ps.

Acc[ording to t](#page-8-0)he reactions 1 and 2 given below, 2 and 8 mol of electrons are consumed for the production of 1 mol of CO and $CH₄$, respectively.

$$
CO2 + 2H+ + 2e- \rightarrow CO + H2O
$$
 (1)

$$
CO_2 + 8e^- + 8H^+ \to CH_4 + 2H_2O
$$
 (2)

The apparent quantum yield (Φ) for the gas products CO and CH_{4} can be calculated according to the following equation:

 $\Phi_{\text{product}}(\%) = (n \text{ mol of product yield/moles of photons})$

absorbed by catalyst) \times 100%

here, $n = 2$ for CO and 8 for CH₄.

For the fresh P25 TiO₂ catalyst, Φ based on the average production yield was calculated to be 0.204% and 0.072% for CO and CH₄, respectively. For the fresh plain $TiO₂$ spheres catalyst, Φ was calculated to be 0.204% and 0.340% for CO and CH₄, respectively. When Pt (i.e., 0.6 wt %) is incorporated, Φ significantly increases up to 1.632% and 1.315% for CO and $CH₄$, respectively.

On the basis of the production rate of the end product $CH₄$ produced, it is interesting to note that the $TiO₂$ spheres catalyst exhibits 4 to 5 times the conversion rate for $CO₂$ reduction that can be obtained by the commercial Degussa P25 TiO₂. Higher photocatalytic activity observed for the plain spherical $TiO₂$ catalyst may be mainly attributed to larger surface area, larger mesoporoous volume, and particularly the hierarchical multimodal pore structure. Usually, for a $TiO₂$ -based photocatalyst, a larger surface area can offer more active adsorption sites and photocatalytic reaction centers. Larger mesoporous volume and the hierarchical pore structure composed of macropores, larger mesopores (ca. 12.4 nm), and smaller mesopores (ca. 2.3 nm) enhance the adsorption efficiency of light and the diffusion of the gas molecules. This behavior has been frequently observed by other researchers. Wang et al. proposed a multiple reflection mechanism and fast mass transport for hierarchically structured photocatalysts.⁵⁵ They claimed that the macrochannels in the hierarchically structured photocatalysts may exhibit two beneficial effe[cts](#page-9-0) on titania, namely, increasing the efficiency of photoabsorption and improving mass transfer. In the macro/ mesoporous $TiO₂$ photocatalyst, the macrochannels could act as a light-transfer path to introduce incident photon flux onto the inner surface of mesoporous $TiO₂$, and enable light to penetrate deep inside the photocatalyst, thus making it a more efficient light harvester. Considering the light absorption, reflection, and scattering within such a hierarchical porous

system, the effective light-activated surface area could be significantly enhanced. The enhanced multiple-light reflection mechanism in hierarchical nanostructured materials was experimentally supported in Wang's paper by the UV−vis DRS of the titanium dioxide materials with/without a hierarchical nanostructure. They also claimed that the transport of small molecules in media featuring large mesopores (>10 nm) and macropores can approach rates of diffusion comparable to those in an open medium, and thus assumed that the macrochannels in their samples can act as effective transport paths for reactants. Such transport enhancement is very important for the application of mesoporous titania in gasphase photocatalysis. In another example, Liu et al. synthesized nanoplates-assembled hierarchical $Bi₂WO₆$ flowers for photocatalysis application.⁵⁶ They claimed that the specific hierarchical configuration, along with the bimodal mesoporous microstructure of the [mu](#page-9-0)ltilayered flower-like assemblies allows multiple scattering of UV−visible light within their frameworks, giving them even greater light-harvesting capacities. The optical path length for light transporting through the $Bi₂WO₆$ hierarchical multilayered flowerlike assemblies may be longer than that for nanoplates due to multiple scattering, resulting in a greater absorbance.

From the literature^{50,56,57} it is very evident that hierarchical nanostructured materials composed of macropores in combination with large m[esopore](#page-9-0)s (>10 nm) can favor improved photoabsorption due to enhanced multiple light refection/ scattering.

Interestingly, in our study it is also evident that the hierarchical nanostructured $TiO₂$ (i.e., the as-synthesized TiO2 microspheres) demonstrate enhanced photoabsorption compared with $TiO₂$ without a hierarchical nanostructure (i.e., P25 $TiO₂$), as shown in Figure 8. This can be attributed to the hierarchical nanostructure composed of macropores (>50 nm) and large mesopores (ca. 12.4 nm) in the as-synthesized $TiO₂$ microsphere catalyst.

Figure 8. UV-vis diffuse reflectance spectra for P25 TiO₂ and the assynthesized TiO₂ microsphere.

In addition, surface defect sites generated during the synthesis process may contribute something to the enhanced photocatalytic activity. Furthermore, the spherical morphology of the $TiO₂$ catalyst can also increase the light scattering during the photocatalytic reaction, and thus can effectively make better use of the UV light, further enhancing the photocatalytic activity.⁵⁷ Generally, after the Pt loading, a 60- to 120-fold increase of H_2 can be generated compared with the plain $TiO₂$ sphere [ca](#page-9-0)talyst, indicating that the H_2 generation reaction through photodriven water splitting is considerably accelerated by Pt. As mentioned previously, H_2 can accelerate the reduction of $CO₂$ to $CH₄$, and as a result, after the Pt loading, $TiO₂$ sphere catalysts also produce higher $CH₄$ than the plain catalyst. In particular, the Pt $(0.6 \text{ wt } %)/TiO₂$ sphere catalyst exhibits the highest production of CH_4 , i.e., ca. 20 times higher CH_4 production than Degussa P25 TiO₂. This value is also more than 2 times higher than that observed for Pt (0.6 wt $%$)/P25 TiO₂.

Although the $TiO₂$ sphere-based catalyst developed here has demonstrated greatly enhanced photocatalytic activity toward photodriven $CO₂$ reduction with water, there is still much potential for further improvement of these catalysts. First, one can synthesize $TiO₂$ spheres with smaller dimensions (e.g., 0.8) and 0.5 mm, Supporting Information) to increase surface area, and with other morphologies, such as hollow $TiO₂$ spheres, in which the h[ollow core can be expect](#page-8-0)ed to facilitate fast mass transport.58−⁶³ Jiao et al. reported that compared with a solid $TiO₂$ crystal, hollow $TiO₂$ crystals and mesocrystals can substanti[ally](#page-9-0) [im](#page-10-0)prove photocatalytic activity (O_2/H_2) evolution from water splitting, CH_4 generation from photoreduction of $CO₂$) as a result of the synergistic effects of a shortened bulk diffusion length for the carriers resulting in decreased bulk recombination, and increased surface area.⁶⁴ Second, it has been reported that Pt particle size plays an important role in the $CO₂$ photoreduction process,⁶⁵ [a](#page-10-0)nd hence, a better synthesis strategy is expected to reduce the particle size of deposited Pt particles, which will enhance [the](#page-10-0) utilization efficiency of the Pt NPs. At present, Pt $(0.6 \text{ wt } %)/TiO₂$ has Pt NPs of ca. 12 nm in size. Large Pt NPs may consume holes, thus serving as recombination centers.⁶⁵ If a better synthesis method is applied, the Pt nanoparticle size is expected to decrease significantly.⁶⁶ With smaller particle s[ize](#page-10-0) and a more uniform dispersion of Pt NPs on the $TiO₂$ substrate, the photocatalytic activity of the [Pt](#page-10-0)loaded $TiO₂$ -based catalysts is expected to improve greatly. Third, some metal elements such as Cu (Fe, Sn) or their oxides can be utilized as co-promoters to further enhance photocatalytic activity of the Pt-loaded $TiO₂$ sphere-based catalyst.

Presently, we have designed and built a photocatalytic UVirradiated (or solar light) fluidized bed reactor with an approximate 0.5 L reactor volume, as shown in Figure S6. The fluidized bed reactor should improve efficiency and scalability of the photocatalytic process using the new $TiO₂$ sphere-based catalysts. Uner et al. reported that a fluidized bed reactor performs better than a fixed bed reactor for $CO₂$ photoconversion and hydrocarbon selectivity because the former has high active surface area and beneficial masstransport conditions.⁶⁷ However, some post-processes were required after use such as filtration, centrifugation, and flocculation to reco[ve](#page-10-0)r powder-type photocatalysts in the slurry. Furthermore, there are some other problems such as the agglomeration, condensation of NPs, and reduced light penetration in the slurry. To solve this problem, we have developed catalysts with a larger particle size (i.e., the asprepared Pt-loaded TiO₂ spheres of ca. 1.3 mm in diameter). The fluidized bed reactor has been used successfully for photocatalytic water splitting,¹⁸ and the plan is to use it for the photocatalytic conversion of $CO₂$ to fuels.

4. CONCLUSIONS

Spherical $TiO₂$ based photocatalysts with large particle size (ca. 1.3 mm) have been developed and explored for photodriven $CO₂$ reduction with water to chemical fuels in singlecompartment batch reactors. It was found that the spherical $TiO₂$ -based catalyst demonstrates much better selectivity to reduce $CO₂$ to the end product, $CH₄$. On the basis of the yield of CH_4 , the spherical TiO₂ catalyst exhibits 4 to 5 times the conversion rate of $CO₂$ reduction that can be obtained by the commercial Degussa P25 TiO₂ catalyst. This is mainly attributable to the superior surface and structural characteristics of the former, i.e., larger surface area and mesoporous volume, and particularly the hierarchical porosity, which is beneficial to fast mass transport and enhanced light harvesting. After Pt loading, the yield of CH₄ is further enhanced. With a Pt loading of 0.6 wt %, the spherical $TiO₂$ -based catalyst exhibits a CH₄ production rate ca. 20 times greater than that produced by Degussa P25 TiO₂, indicating that the spherical TiO₂-based catalysts are very promising for photodriven $CO₂$ reduction. There is also significant potential for further improvement of the photocatalytic performance for spherical $TiO₂$ -based catalysts. Approaches would include using hollow $TiO₂$ spheres, depositing Pt NPs with smaller particle size, and incorporating Cu (Fe, Sn) as a co-promoter. Some of the work involving these approaches is already in progress. In addition to the study with the batch reactors, we have also developed a fluidized bed reactor, which can be used for scalable $CO₂$ reduction and $H₂O$ splitting processes. The spherical based photocatalysts with particle size greater than several hundreds of micrometers are ideally suited to these scalable processes.

■ ASSOCIATED CONTENT

6 Supporting Information

Photographs for the experimental setup, SEM images for $TiO₂$ spheres with various particle size, SEM images for commercial Degussa P25 TiO₂, SEM images for the Pt $(1.8 \text{ wt } \%) / TiO₂$ spheres, the XRD pattern for Pt black, and a photograph for a photocatalytic UV-irradiated fluidized bed reactor. This material is available free of charge via the Internet at http://pubs. acs.org.

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The authors declare no competing fi[nancial interest.](mailto:dwilkinson@chbe.ubc.ca)

■ ACKNOWLEDGMENTS

The authors would like to thank Carbon Management Canada (CMC project B222) and the Pacific Institute for Climate Solutions (PICS) for financial support, and to thank Dr. Alfred Lam and Greg Afonso for help with designing and fabricating the reactors.

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